## Thermodynamics of Charge-unsymmetrical Anion Mixtures. II. The Liquid Systems $AF - A_2MoO_4$ and $AF - A_2WO_4$

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The thermodynamic properties of the liquid mixtures  $AF - A_2MOO_4$  and  $AF - A_2WO_4$  (A = Li, Na, K) have been studied by calorimetric and cryoscopic measurements. When the partial Gibbs energies, derived from the phase diagrams, are compared with partial enthalpies from calorimetry, we obtain precise information on the partial entropies of mixing. These entropies generally are larger than calculated from the Temkin model. The results are discussed in terms of a Flory-type model for monovalent—divalent mixtures, and of the size parameters of the salts. The heat of fusion of  $K_2MoO_4$  was not known and has been measured. It was found to be 34.7 + 0.7 kJ/mol.

In a recent communication 1 we have discussed the thermodynamic properties of alkali fluoride-alkali sulfate mixtures. In that study the partial entropies of the two components derived from cryoscopic and calorimetric data were compared with configurational entropies calculated from several quasilattice models proposed by Førland.<sup>2</sup> It was found that these mixed anion - common cation systems have entropies of mixing which are predicted quite well by a Flory-type model, in which the divalent sulfate ion occupies two anion positions in a quasi-lattice of the Temkin type. However, the calorimetric measurements on the fluoride-sulfates did not provide a clear answer to the question of whether the enthalpies of mixing in these charge-unsymmetrical systems can be represented better by an equation based on equivalent fractions than on mol fractions.

In order to investigate such charge-unsymmetrical mixtures in greater detail we have extended our study to the fluoride – molybdate and fluoride –

tungstate systems. Since the  $MoO_4^{2-}$  and  $WO_4^{2-}$  anions are considerably larger than  $SO_4^{2-}$ , it was hoped that this would throw light on the influence of the size of the divalent anion on the thermodynamic properties.

The phase diagrams of the alkali fluoride—molybdate and fluoride—tungstate systems are available.<sup>3-7</sup> However, as for fluoride—sulfate, we found that the cryoscopic data were not sufficiently accurate to provide reliable Gibbs energy information. For this reason the phase diagrams were reinvestigated.

## **EXPERIMENTAL**

Cryoscopic measurements. These measurements were carried out by monitoring the cooling curves of the mixtures in the manner described previously. The composition of the melts was changed by adding weighed amounts of crystals (fluorides) or pellets (molybdates and tungstates) through a feeding tube. The maximum absolute error in the measured liquidus temperatures was esitmated to be  $\pm 2\,^{\circ}\mathrm{C}$ . However, the freezing point depressions, relative to the melting point of the pure salts, in most cases, could be measured to about  $\pm 0.3\,^{\circ}\mathrm{C}$ .

Calorimetric measurements. The calorimetric measurements were performed in a Calvet-type twin microcalorimeter which has been described elsewhere. The mixing experiments were of the liquid—liquid type and were carried out in an argon atmosphere at 1273 K. The procedures were similar to those used previously.

We found enthalpy of fusion data in the literature for all salts studied except for potassium molybdate. In order to secure this information we carried out a series of calorimetric measurements in which solid potassium molybdate was dissolved in a liquid

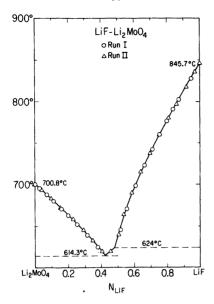


Fig. 1. Liquidus curves for the phase diagram LiF—Li<sub>2</sub>MoO<sub>4</sub>.

mixture of potassium molybdate ( $\sim$ 85%) and potassium fluoride ( $\sim$ 15%) at 1180 K, *i.e.*, about 20°C below the melting point of potassium molybdate. The enthalpy of fusion was then obtained

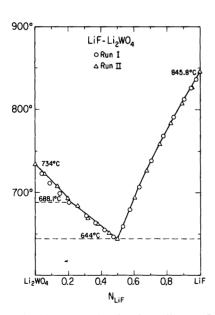


Fig. 2. Liquidus curves for the phase diagram  $LiF-Li_2WO_4$ .

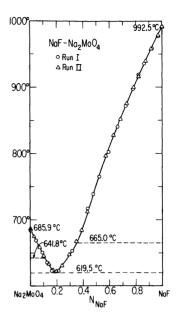


Fig. 3. Liquidus curves for the phase diagram  $NaF-Na_{2}MoO_{4}$ .

by correcting for the small liquid—liquid heat of mixing. In other ways the experimental procedures were similar to those used in the liquid—liquid

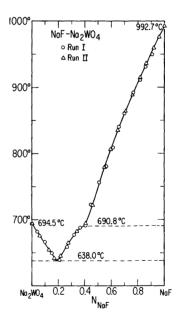


Fig. 4. Liquidus curves for the phase diagram NaF — Na<sub>2</sub>WO<sub>4</sub>.

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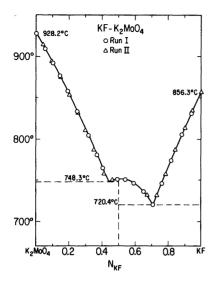


Fig. 5. Liquidus curves for the phase diagram  $KF - K_2MoO_4$ .

mixing experiments. A preliminary survey of the data for the  $Na_2MoO_4-NaF$  and  $Li_2WO_4-LiF$  mixtures indicated that the partial entropies of the molybdate and tungstate in these two systems differed from all the other entropy data. For this reason the enthalpies of fusion of  $Na_2MoO_4$  and of  $Li_2WO_4$  were redetermined using the same procedure as for  $K_2MoO_4$ .

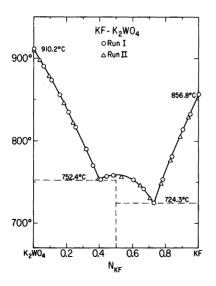


Fig. 6. Liquidus curves for the phase diagram  $KF - K_2WO_4$ .

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In our calorimetric measurements as 1253 K the calorimeter was calibrated electrically as described previously, with a precision of about  $\pm 0.6$ %. In the other calorimetric measurements we used a drop calibration based on the heat content equation for platinum recommended by Kelley. 15

Chemicals. The chemicals used were: LiF, Fisher Certified Reagent (min. 99.5 %); LiMoO<sub>4</sub>, Research Inorganic/Organic Chemicals (99.5 %); Li<sub>2</sub>WO<sub>4</sub>, for calorimetric work: Research Inorganic/Organic Chemicals (99%), for cryoscopy: Research Inorganic/Organic Chemicals (99.9%); NaF, Baker Analyzed Reagent (min. 99 %); Na<sub>2</sub>MoO<sub>4</sub>, Baker Analyzed Reagent (Na<sub>2</sub>MoO<sub>4</sub>· 2H<sub>2</sub>O, 101 %); Na<sub>2</sub>WO<sub>4</sub>, Apache Chemicals, Inc. (Na<sub>2</sub>WO<sub>4</sub>· 2H<sub>2</sub>O, Folin grade); KF, Baker and Adamson, Anhydrous Granular Reagent (min. K<sub>2</sub>MoO<sub>4</sub>, Research Inorganic/Organic Chemicals (99.9 %). The chemicals were dried overnight in vacuum at 150 °C. The fluorides used in the cryoscopic work were melted in an inert, dry atmosphere, after which clear crystals were picked from the solidified melts.

## RESULTS AND DISCUSSION

Cryoscopic data. The experimental results are presented graphically in Figs.1-6; liquidus temperatures for round figure and eutectic compositions are summarized in Tables 1-6.

Our liquidus curves show general agreement with the previously published phase diagrams; even so, numerical discrepancies in some cases are quite substantial. Note that the two potassium systems have congruently melting 50 – 50 interstitial compounds, while the two sodium systems have compounds of the same composition which melt incongruently. In LiF-Li<sub>2</sub>MoO<sub>4</sub> we found indication of an incongruently melting compound of a somewhat different composition. This compound was not reported by Schmitz-Dumont and Weeg.<sup>3</sup> However, Karov and Bilokov 7 found evidence for its existence and suggested that its composition is Li<sub>2</sub>MoO<sub>4</sub> · 2LiF. Unfortunately, our cryoscopic data do not allow us to draw firm conclusions regarding its stoichiometry.

In contrast to this, the corresponding LiF-Li<sub>2</sub>WO<sub>4</sub> binary is of the simple eutectic types. Note, however, that the tungstate-rich part of this diagram may be less accurate than the other cryoscopic data. As discussed below, the phase transition in Li<sub>2</sub>WO<sub>4</sub> at 688 °C is very slow. Therefore, it is very difficult to obtain equilibrium cryscopic data by the thermal analysis procedure which was used.

Table 1. Partial thermodynamic data for the liquid system LiF-Li<sub>2</sub>MoO<sub>4</sub>.

$N_{ m LiF}$	$egin{array}{c} T_{ m liq} \ { m K} \end{array}$	$\Delta \overline{G}_{ m LiF}$ J mol $^{-1}$	$rac{\Delta \overline{H}_{ m LiF}}{ m J~mol^{-1}}$	$\Delta \overline{S}_{LiF}$ J mol <sup>-1</sup> K <sup>-1</sup>	$\Delta \overline{S}_{LiF}^{E}$ J mol <sup>-1</sup> K <sup>-1</sup>
1.0	1118.9		_	-	_
0.90	1084.4	-821.7	250.4	0.99	0.11
0.80	1049.0	-1662.5	842.6	2.39	0.53
0.70	1011.6	-2570.6	1571.6	4.07	1.11
0.60	968.4	-3570.6	2277.1	6.04	1.79
0.50	909.4	-4964.6	2843.4	8.59	2.83
0.482	897.2 Peritec	t.			
		$\Delta \overline{G}_{ ext{Li}_2 ext{MoO}_4}$	$\Delta ar{H}_{ ext{Li}_2 ext{MoO}_4}$	$\Delta \overline{S}_{\text{Li}_2\text{MoO}_4}$	$\Delta \overline{S}^{\mathrm{E}}_{\mathrm{Li}_{2}\mathrm{MoO}_{4}}$
0.435	887.5 Eut.	-4277.8	50.9	4.88	0.13
0.40	894.0	-3962.2	-19.8	4.41	0.16
0.30	916.2	-2876.6	-89.5	3.04	0.08
0.20	936.4	-1878.9	-59.7	1.94	0.09
0.10	955.7	-917.7	-16.2	0.94	0.07
0.0	974.0	_	_	_	_

Table 2. Partial thermodynamic data of LiF in the liquid system LiF-Li<sub>2</sub>WO<sub>4</sub>.

$N_{ m LiF}$	$_{ m K}^{T_{ m liq}}$	$\Delta \overline{G}_{ m LiF}$ J mol <sup>-1</sup>	$\Delta \overline{H}_{ m LiF}$ J mol $^{-1}$	$\Delta \overline{S}_{LiF}$ J mol <sup>-1</sup> K <sup>-1</sup>	$\Delta \overline{S}_{LiF}$ J mol <sup>-1</sup> K <sup>-1</sup>
1.00	1119.0	_	_	_	_
0.90	1084.2	-828.7	224.9	0.97	0.10
0.80	1048.0	-1688.4	758.3	2.33	0.48
0.70	1009.8	-2593.5	1419.0	3.97	1.01
0.60	965.0	-3653.0	2066.5	5.93	1.68
0.50	918.2	-4758.6	2600.9	8.02	2.26
0.498	917.4 Eut.	-4777.5	2610.0	8.05	2.26

Table 3. Partial thermodynamic data for the liquid system NaF-Na<sub>2</sub>MoO<sub>4</sub>.

$N_{ m NaF}$	$_{ m K}^{T_{ m liq}}$	$\Delta \overline{G}_{ m NaF}$ $ m J~mol^{-1}$	$\Delta \overline{H}_{\mathrm{NaF}}$ J mol $^{-1}$	$\Delta \overline{S}_{NaF}$ J mol <sup>-1</sup> K <sup>-1</sup>	$\Delta \overline{S}_{NaF}^{E}$ J mol <sup>-1</sup> K <sup>-1</sup>
1.0	1265.7		_	_	_
0.90	1224.5	-866.0	167.1	0.84	-0.03
0.80	1179.6	-1803.8	542.5	1.99	+0.13
0.70	1133.2	-2767.1	974.1	3.30	0.34
0.60	1082.8	-3807.8	1358.5	4.77	0.53
0.50	1024.7	-5001.6	1641.7	6.48	0.72
0.40	963.2	-6260.8	1818.2	8.39	0.77
0.353	938.2 Peritect.	-6772.0	1875.0	9.22	0.56
		$\Delta \overline{G}_{\mathrm{Na_2MoO_4}}$	$\Delta \overline{H}_{\mathrm{Na_2MoO_4}}$	$\Delta \overline{S}_{\mathrm{Na_2MoO_4}}$	$\Delta \overline{S}^E_{Na_2MoO_4}$
$0.19_{0}$	892.7 Eut.	-2029.8	79.8	2.36	0.61
0.10	919.2	-882.9	31.9	1.00	0.13
0.00	959.1	_			

$N_{\rm NaF}$	$egin{array}{c} T_{ m liq} \ { m K} \end{array}$	$\Delta \overline{G}_{ m NaF}$ J mol $^{-1}$	$\Delta \overline{H}_{\mathrm{NaF}}$ J mol <sup>-1</sup>	$\Delta \overline{S}_{NaF}$ J mol <sup>-1</sup> K <sup>-1</sup>	$\Delta \overline{S}_{NaF}^{E}$ J mol <sup>-1</sup> K <sup>-1</sup>
1.0	1265.9	_	_	_	_
0.90	1224.1	-878.4	157.6	0.85	-0.03
0.80	1179.7	-1805.6	518.1	1.97	+0.12
0.70	1133.0	-2774.9	943.0	3.28	0.32
0.60	1081.7	-3833.9	1333.8	4.78	0.53
0.50	1021.0	-5080.7	1631.9	6.57	0.81
0.40	964.0 Peritect.	-6247.5	1818.7	8.37	0.75
		$\Delta \overline{G}_{Na_2WO_4}$	$\Delta \overline{H}_{\mathrm{Na_2WO_4}}$	$\Delta \overline{S}_{Na_2WO_4}$	$\Delta \overline{S}^{\rm E}_{{ m Na_2WO_4}}$
0.185	911.2 Eut.	-1622.0	37.8	1.82	0.12
0.10	937.4	-872.2	16.4	0.95	0.07
0.00	967.7	_	_	_	

Table 4. Partial thermodynamic data for the liquid system NaF-Na<sub>2</sub>WO<sub>4</sub>.

Table 5. Partial thermodynamic data for the liquid system KF-K<sub>2</sub>MoO<sub>4</sub>.

$N_{\mathrm{KF}}$	$_{ m K}^{T_{ m liq}}$	$\Delta \overline{G}_{ m LiF} \  m J~mol^{-1}$	$\Delta \overline{H}_{\mathrm{KF}}$ J mol <sup>-1</sup>	$\Delta \overline{S}_{KF}$ J mol <sup>-1</sup> K <sup>-1</sup>	$\Delta \widehat{S}_{KF}^{E}$ J mol <sup>-1</sup> K <sup>-1</sup>
1.00	1129.5	_	_	_	_
0.90	1085.7	-1144.0	9.1	1.06	0.19
0.80	1038.7	-2371.8	36.3	2.32	0.46
0.708	993.6 Eut. I	-3550.2	77.3	3.65	0.78
0.70	995.7	_	_	_	_
0.60	1018.7	_	_	_	***
0.50	1025.0		_	_	-
		$\Delta \overline{G}_{\mathrm{K_2MoO_4}}$	$\Delta \overline{H}_{\mathrm{K_2MoO_4}}$	$\Delta \overline{S}_{K_2MoO_4}$	$\Delta \overline{S}^{\rm E}_{{ m K_2MoO_4}}$
0.44	1021.6 Eut. II	-5003.9	279.9	5.17	0.35
0.40	1039.7	-4537.2	142.7	4.50	0.26
0.30	1084.7	-3326.9	80.1	3.14	0.18
0.20	1127.7	-2121.9	35.5	1.91	0.06
0.10	1166.0	-1024.8	8.9	0.89	0.01
0.00	1201.5	-	_	_	

Enthalpy data. The results of the calorimetric mixing measurements are presented in Fig. 7, which shows plots against composition of the enthalpy interaction parameters,  $\lambda_{\rm m}$ , defined as  $\lambda_{\rm m} = \Delta H_{\rm mix}/N_1N_2$ ;  $N_1$  and  $N_2$  are the mol fractions of the two components. We found that  $\lambda_{\rm m}$  could be fitted to simple polynomials, eqn. (1). Values of the coefficients a, b, and c determined by a least squares

$$\lambda_{\rm m} = a + bN_1 + cN_1^2 \tag{1}$$

treatment of the experimental data are listed in Table 7. Note that the relative partial enthalpies of

the two components can be calculated from eqns. (2a) and (2b), where a, b, and c are the parameters in eqn. (1).

$$\Delta \overline{H}_1 = (a + 2bN_1 + 3cN_1^2)(1 - N_1)^2$$
 (2a)

$$\Delta \overline{H}_2 = (a - b + 2(b - c)N_1 + 3cN_1^2)N_1^2$$
 (2b)

According to simple quasi-lattice theory the enthalpy interaction parameter should be independent of composition. This seems to hold well for the potassium fluoride—molybdate and fluoride—tungstate mixtures. However, it clearly does not

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$N_{KF}$	T <sub>liq</sub> K	$\Delta \overline{G}_{KF}$ J mol <sup>-1</sup>	$\Delta \overline{H}_{\mathrm{KF}}$ J mol $^{-1}$	$\Delta \overline{S}_{KF}$ J mol <sup>-1</sup> K <sup>-1</sup>	$\Delta \overline{S}^{E}_{KF}$ J mol <sup>-1</sup> K <sup>-1</sup>
1.00	1129.9	_		_	_
0.90	1084.2	-1193.2	11.1	1.11	0.24
0.80	1036.2	-2446.7	42.5	2.40	0.55
0.728	997.5 Eut. I	-3457.5	77.0	3.54	0.91
0.70	1005.7	_	_	_	_
0.60	1026.4	-		_	
0.50	1031.7	-	_	-	_
		$\Delta \overline{G}_{K_2WO_4}$	$\Delta \overline{H}_{\mathrm{K_2WO_4}}$	$\Delta \overline{S}_{\kappa_2 w o_4}$	$\Delta \overline{S}^{E}_{K_{2}WO_{4}}$
0.40	1025.6 Eut. II	<b>-4547.7</b>	97.6	4.53	0.28
0.30	1069.2	-3340.7	50.4	3.17	0.21
0.20	1111.6	-2119.7	20.4	1.93	+0.07
0.10	1150.0	-990.1	4.6	0.86	-0.01
0.00	1183.4	_	_	<u> </u>	

Table 6. Partial thermodynamic data for the liquid system KF-K<sub>2</sub>WO<sub>4</sub>.

apply for the corresponding lithium and sodium systems, which show much larger positive interaction parameters in the fluoride-rich than in the molybdate and tungstate-rich regions.

Førland <sup>2</sup> developed a quasi-lattice theory for charge-unsymmetrical fused salt mixtures based on equivalent fractions rather than on mol fractions. In this theory the enthalpy interaction parameter has the form (3), where  $N_1$  is the mol fraction of the

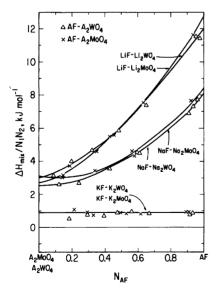


Fig. 7. Plots of enthalpy interaction parameters,  $\lambda_m$ , for AF – A<sub>2</sub>MoO<sub>4</sub> and AF – A<sub>2</sub>WO<sub>4</sub>.

$$\lambda_{\rm m} = \Delta H_{\rm mix} / (N_1 + 2N_2) (N_1 N_2) \tag{3}$$

monovalent salt,  $N_2$  the mol fraction of the divalent salt, while  $N_1$  and  $N_2$  are the respective equivalent fractions (4a) and (4b). The results are plotted according to eqn. (3) in Fig. 8.

$$N_1 = N_{AF} = n_{AF}/(n_{AF} + 2n_{A2XO_4})$$
 (4a)

$$N_2' = N_{A_2XO_4}' = 2n_{A_2XO_4}/(n_{AF} + 2n_{A_2XO_4})$$
 (4b)

In our earlier paper we presented the enthalpy of mixing data for the AF-A<sub>2</sub>SO<sub>4</sub> system in the same

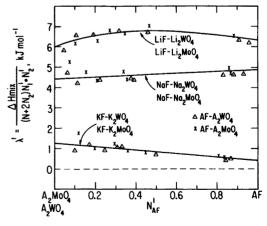


Fig. 8. Plots of enthalpy interaction parameters,  $\lambda_{m}'$ , for AF-A<sub>2</sub>MoO<sub>4</sub> and AF-A<sub>2</sub>WO<sub>4</sub>.

System	a, J mol <sup>-1</sup>	b, J mol <sup>-1</sup>	c, J mol <sup>-1</sup>
LiF-Li <sub>2</sub> MoO <sub>4</sub>	2672	4044	6210
LiF-Li <sub>2</sub> WO <sub>4</sub>	2936	3225	5657
NaF-Na <sub>2</sub> MoO <sub>4</sub>	3067	-1601	6801
$NaF - Na_2^2WO_4$	2483	-121	5554
$KF - K_2MoO_4$	894	9	_
$KF - K_2^2WO_4$	660	251	_

Table 7. Summary of experimentally determined coefficients according to Eqn. (1).

manner. However, for those systems it was not evident that the equivalent fraction representation (eqn. (3)) was preferable to the mol fraction representation. Fig. 8 shows that this situation is different for the molybdate—fluoride and tungstate—fluoride mixtures; we see that the plots of  $\lambda_m'$  against N' are much more symmetrical than plots of  $\lambda_m$  against N.

From our measurements on  $K_2MoO_4$  we found that the enthalpy of fusion of this salt at the melting point,  $\Delta H_m(K_2MoO_4)$  is 34.7 kJ mol<sup>-1</sup> with an estimated uncertainty of 0.7 kJ mol<sup>-1</sup> ( $\pm 2 \%$ ).

We also measured the heats of fusion of Na<sub>2</sub>MoO<sub>4</sub> and LiWO<sub>4</sub> a few degrees below their respective melting points; this yielded the values  $20.4 \pm 0.4$ kJ mol<sup>-1</sup> and 40.3±0.8 kJ mol<sup>-1</sup>, respectively. In order to obtain information on the enthalpy change associated with the solid state phase transformations in these salts we measured also the heats of fusion below the phase transformation temperature. We found for Na<sub>2</sub>MoO<sub>4</sub> at 641.0 °C 28.7  $\pm$  0.4 kJ mol<sup>-1</sup>, and for LiWO<sub>4</sub> at 687.0 °C  $50.8 \pm 1.0$  kJ mol<sup>-1</sup>. If heat capacity terms are neglected, we find for the phase transformation in Na<sub>2</sub>MoO<sub>4</sub> 28.7-20.4= 8.3 kJ mol<sup>-1</sup> and in Li<sub>2</sub>WO<sub>4</sub> 50.8-40.3=10.5 kJ mol<sup>-1</sup>. For Na<sub>2</sub>MoO<sub>4</sub> our results are in good agreement with the literature,11 which gives 21.42 kJ mol<sup>-1</sup> and 8.28 kJ mol<sup>-1</sup> for the heat of fusion and phase transformation, respectively. For Li<sub>2</sub>WO<sub>4</sub>, on the other hand, we find good agreement for the heat of fusion near the melting point (41.0 kJ mol<sup>-1</sup> from Ref. 10), but a wide discrepancy for the heat of transformation (2.0 kJ mol<sup>-1</sup>, compared to our calculated result of 10.5 kJ mol<sup>-1</sup>). However, if we take the heat capacity difference between solid and liquid into account (Ref. 10), this latter discrepancy is largely eliminated.

The very strong temperature dependence of the heats of fusion and transformation in Li<sub>2</sub>WO<sub>4</sub> suggests that the phase transformation in Li<sub>2</sub>WO<sub>4</sub>

at 688 °C is not a simple first order transformation, but extends over a range of temperatures, It is also possible that earlier measurements on this substance by drop calorimetry may not have yielded true equilibrium values.

Partial entropies. The partial Gibbs energy of component A in solution can be calculated from the liquidus by means of eqn. (5).<sup>13</sup>

$$-\Delta \overline{G}_{A} = \Delta G_{A,S-L}(T) = \Delta H_{m}(1 - \frac{T}{T_{m}}) - a[(T_{m} - T) - T \ln \frac{T_{m}}{T}] - \frac{b}{2}(T_{m} - T)^{2} - \frac{1}{2}cT(\frac{1}{T_{m}} - \frac{1}{T})^{2}$$
 (5)

The standard state of component A here is the pure undercooled liquid;  $\Delta H_{\rm m}$  is the enthalpy of fusion of A at its melting point,  $T_{\rm m}$ ; T is the liquidus temperature. The coefficients a, b, and c are constants in the analytical expression for the heat capacity difference between solid and undercooled liquid, eqn. (6).

$$\Delta C_{p,s-1} = C_1 - C_s = a + bT + c/T^2 \tag{6}$$

In applying eqn. (5) it is assumed that solid solubility is negligible; in view of the difference in the charge and size of the anions this is a very reasonable assumption. When the solid undergoes a phase transformation in the temperature range of interest, the calculation of  $\Delta \overline{G}_A$  may still be performed if the enthalpy and entropy changes in the phase transformation are taken into account.<sup>1</sup>

If we make the further assumption that the enthalpy of mixing is independent of temperature in the considered temperature range, we can calculate the partial entropies of A along the liquidus curve from  $\Delta \bar{G}_{\rm A}$  and  $\Delta \bar{H}_{\rm A}$ . Fig. 9 presents graphs of the calculated partial excess entropies with respect to the Temkin model. Previously published values

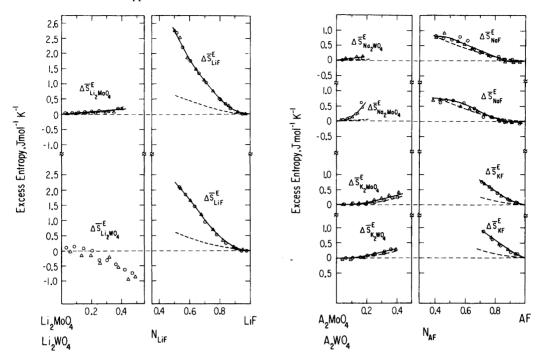


Fig. 9. Plots of partial excess and entropies for  $AF - A_2MoO_4$  and  $AF - A_2WO_4$  systems based on the Temkin model for the ideal entropy of mixing. The two symbols represent data based on runs I(0) and II( $\Delta$ ) of the cryoscopic measurements. The broken lines represent excess partial entropies calculated from a Flory-type model (see text).

Table 8. Enthalpy and heat capacity data used in calculations of partial Gibbs energies.

Salt	$\Delta H_{ m m}$	$\Delta C_{p_{e-1}}$	Ref.
	J mol <sup>-1</sup>	$\frac{\Delta C_{p_{S}-1}}{J\;mol^{-1}\;K^{-1}}$	
LiF	26,690	$-10.16+11.72\times10^{-3}T-\frac{591913}{T^2}$	9
Li <sub>2</sub> MoO <sub>4</sub>	49,000	96.4 - 0.0823T	10
Li <sub>2</sub> WO <sub>4</sub>	$2,000 (\Delta H_{\rm tr})$	$-5874 + 6.102 \text{T} (\Delta C_{\text{pl-II}})$	10
	41,000	5973 – 6.180 <i>T</i>	
NaF	33,470	$0.51 - 0.43 \ 10^{-3} - \frac{31836}{T^2}$	9
Na <sub>2</sub> MoO <sub>4</sub>	$8,280 (\Delta H_{tr})$	$405.17 - 184.5 \ 10^{-2} T (\Delta C_{p_1-1})$	11ª
	21,420	$-892.4+95.4\ 10^{-2}T$	
Na <sub>2</sub> WO <sub>4</sub>	27,870	$245.6 - 25.58 \ 10^{-2} T$	11
KF	29,500	$-0.29 + 0.159 \ 10^{-3} T - \frac{23059}{T^2}$	9
K <sub>2</sub> MoO <sub>4</sub>	34,700	See text.	This work
$K_2WO_4$	35,100	$300.98 - 25.58 \times 10^{-2}T$	10

<sup>&</sup>lt;sup>a</sup> C<sub>p</sub> data in Ref. 11 have been used. Equations in this reference contain printing errors.

of  $\Delta H_{\rm m}$  and  $\Delta C_{\rm p}$  are summarized in Table 8. For  ${\rm Li_2WO_4}$  we adopted our own values of the heats of fusion and transformation, and did not take any  $\Delta C_{\rm p}$  contribution into account. Since the character of the solid state phase transformation is uncertain, any attempt to include heat capacity terms in the calculation would be of very doubtful value.

As no information is available on  $\Delta C_p$  for  $K_2MoO_4$ , we adopted for this salt the known data for  $K_2WO_4$ . These salts have very similar melting points and heats of fusion. Furthermore, the  $\Delta C_p$  term represents only a minor correction term.

From Fig. 9 we see that the partial excess entropies of the alkali fluorides in fluoride-rich mixtures are very nearly the same for molybdates and tungstates. However, among the molybdate- and tungstate-rich solutions we note that the data for Li<sub>2</sub>WO<sub>4</sub> deviate significantly from the results for the other systems. We believe this is probably due to inaccuracies in the cryoscopic data, possibly caused by the sluggish character of the phase transformation in Li<sub>2</sub>WO<sub>4</sub>. Note also that it will be very difficult to reconcile the calculated partial entropies of LiF and Li<sub>2</sub>WO<sub>4</sub> in this system with the Gibbs-Duhem relation.

In our earlier paper on fluoride-sulfate mixtures we discussed the various pseudo-lattice models for charge-unsymmetrical fused salt systems proposed by Førland.<sup>2</sup> The model which best predicted the observed entropies of mixing in these systems is based on the assumption that the divalent sulfate ion replaces two mono-valent fluoride ions in the anion "sub-lattice." In this model the entropy of mixing will be the same as for a mixture of monomers and dimers according to the theory of Flory: <sup>14</sup>

$$\Delta S_{\text{mix}} = -R(n_{\text{AF}} \ln N_{\text{AF}}^{'} - n_{\text{A}_{2}\text{XO}_{4}} \ln N_{\text{A}_{2}\text{XO}_{4}}^{'})$$
 (7a)

$$\Delta \overline{S}_{AF} = -R \ln N'_{AF} - \frac{1}{2}RN'_{A_{2}XO_{4}}$$
 (7b)

$$\Delta \overline{S}_{A_2XO_4} = -R \ln N_{A_2XO_4} + RN_{AF}$$
 (7c)

In Fig. 9 we have included graphs of the partial excess entropies calculated from this model for comparison with the experimental data. For solutions rich in molybdate and tungstate we see that the agreement generally is very good. For fluoriderich solutions, on the other hand, a more detailed analysis will be attempted. For solutions of potassium tungstate and molybdate in potassium fluoride the observed excess entropies are considerably larger than calculated from the model; the entropies are

also slightly larger than for sulfate in fluoride: at  $N_{\rm KF} = 0.8$  we have  $\Delta \overline{S}_{\rm KF}^{\rm K}$  (molybdate and tungstate)  $\approx 0.5$  J mol<sup>-1</sup> K<sup>-1</sup>, as compared to  $\Delta \overline{S}_{\rm KF}$  (sulfate)  $\approx 0.4$  J mol<sup>-1</sup> K<sup>-1</sup>.

The partial enthalpies of sodium fluoride in fluoride-rich mixtures with tungstate and molybdate agree very well with the model; in these cases, however, the observed excess entropies are significantly smaller than for sodium fluoride—sulfate: at  $N_{\rm NaF}\!=\!0.6$ , we have  $\Delta \overline{S}_{\rm NaF}^{\rm E}$  (molybdate and tungstate)  $\approx 0.55~\rm J~mol^{-1}~K^{-1}$ , as compared to  $\Delta \overline{S}_{\rm NaF}^{\rm E}$  (sulfate)  $\simeq 1.0~\rm J~mol^{-1}~K^{-1}$ .

For solutions rich in lithium fluoride the situation is reversed: at  $N_{\rm LiF}$ =0.6, we have  $\Delta \overline{S}_{\rm LiF}^{\rm E}$  (molybdate and tungstate)  $\simeq 1.75~\rm J~mol^{-1}~K^{-1}$ , and  $\Delta \overline{S}_{\rm LiF}^{\rm E}$  (sulfate)  $\simeq 0.8~\rm J~mol^{-1}~K^{-1}$ .

In order to rationalize these results let us consider in somewhat greater detail the size relations in the considered binary mixtures. For anion mixtures, in which a large divalent ion replaces two small singly charges ions, it is expected that the anion—anion separation in the salt with the smaller anion should be the size parameter of principal interest. Such information on the considered fluorides is available from the X-ray diffraction work of Zarzycki. 12 For the considered divalent anions the choice of an appropriate size parameter is more uncertain since we do not know to what extent the anions are free to rotate in the melts. Lacking such information, we arbitrarily adopt the radius of free rotation of the XO<sub>4</sub><sup>2</sup> ions; this is about 2.9 Å for sulfate, and about 3.3 Å for molybdate and tungstate. It we now compare the fluoride-fluoride distances in the salts with  $r_{XO_4}^2$ -, the following picture emerges:

For the potassium systems:

$$\frac{r_{\text{SO}_4^{2^-}}}{d_{\text{E}^--\text{E}^-}} = \frac{2.9 \text{ Å}}{3.86 \text{ Å}} = 0.75$$

$$\frac{r_{\text{XO}4^{2^-}}}{d_{\text{F}^--\text{F}^-}} = \frac{3.3}{3.86} = 0.85$$

For the sodium systems:

$$\frac{r_{\text{SO_4}^2}}{d_{\text{F}^-\text{F}^-}} = \frac{2.9 \,\text{Å}}{3.44 \,\text{Å}} = 0.84$$

$$\frac{r_{\text{XO}_4}^2}{d_{\text{E}^--\text{E}^-}} = \frac{3.3}{3.94} = 0.96$$

For the lithium systems:

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$$\frac{r_{\text{SO}_4^{2^-}}}{d_{\text{F}^--\text{F}^-}} = \frac{2.9 \,\text{Å}}{2.9 \,\text{Å}} = 1.0$$

$$\frac{r_{\text{XO4}^{2-}}}{d_{\text{F}^--\text{F}^-}} = \frac{3.3}{2.9} = 1.14$$

Of course, it is not possible to draw entirely firm conclusions from a comparison of these size ratios. Even so, our results indicate that when the ratio  $r_{\text{XO}_4}^2 - /d_{\text{F}^- - \text{F}^-}$  is close to 1, the partial entropies of fluoride in the fluoride-rich solutions agree reasonably well with the Flory model. This is the case, for example, for NaF – Na<sub>2</sub>WO<sub>4</sub> and NaF – Na<sub>2</sub>MoO<sub>4</sub>, and also for LiF – Li<sub>2</sub>SO<sub>4</sub>.

On the other hand, when this ratio is either larger than 1 (i.e., LiF-Li<sub>2</sub>WO<sub>4</sub> and LiF-Li<sub>2</sub>MoO<sub>4</sub>) or significantly lower than 1 (i.e., KF-K<sub>2</sub>SO<sub>4</sub>), the excess entropies tend to be larger than calculated from the Flory model. These additional entropy terms may be either configurational and/or vibrational in character; they may even to some extent be related to the freedom of rotation of the XO<sub>4</sub><sup>2-1</sup> anions. Since the model accounts fairly well for the general trend of the excess entropies, the differences from cation to cation probably are largely of a vibrational origin.

It seems to us highly probable that the model will break down when the considered size ratio differs very significantly from 1. In this context we believe it would be of considerable interest to obtain reliable entropy data for oxide—fluoride mixtures. It also would be of special interest to study fused salt mixtures in which the small, singly charged fluoride anion is mixed with anions of higher charge than 2, such as, e.g.,  $F^- - PO_4^{3-}$  and  $F^- - VO_4^{3-}$  mixtures.

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