Kinetic Studies of the Hydrolysis of Aromatic Sulphonic Anhydrides

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The solvolysis of various aromatic sulphonic anhydrides in aqueous acetone and dioxan has been studied kinetically using a stopped-flow apparatus. The reaction mechanism is found to be an $\rm S_{N}2$ hydrolysis. The experimental data are compared with literature data for solvolysis of corresponding sulphonyl chlorides in similar solvents, for which an $\rm S_{N}2$ mechanism also has been established. The higher rates of solvolysis of sulphonic anhydrides compared with sulphonyl chlorides are mainly caused by higher values of the activation entropy.

The solvolysis of sulphonates, RSO₂R', and of sulphonyl chlorides, RSO₂Cl, have been extensively studied in the past,¹ but no report appears to exist on the solvolysis of sulphonic anhydrides, (RSO₂)₂O. A similar situation does not exist with respect to the carboxyl analogues, RCOOR', RCOCl, and (RCO)₂O.

The sulphonic anhydrides form a class of compounds of special interest. They are known to be very reactive, and in certain respects superior as derivating reagents compared to the sulphonyl chlorides.²⁻⁴ Furthermore, they appear as intermediates in aprotic aromatic sulphonation, a fact with both practical and theoretical consequences.^{5,6}

In this paper a report is given of kinetic studies on the hydrolysis of aromatic sulphonic anhydrides in mixtures of water and acetone or dioxan in a temperature range from 15 to 40°. The reactions were followed by conductometric measurements. The fairly high rate of reaction necessitated the use of a stopped-flow apparatus with automatic recording of the conductivity.

EXPERIMENTAL

Materials. Acetone was fractionated over potassium permanganate. Dioxan was refluxed over sodium for several hours and finally distilled. Water was distilled twice. p-Toluene sulphonic anhydride was prepared from the corresponding acid monohydrate according to Thuneberg. The monohydrate (Fluka) was transformed into the

anhydrous acid by evaporation in vacuo at 120° . The residue was treated with 4-6weights of thionyl chloride at 90°. After having removed the excess of thionyl chloride the residue was recrystallised several times from benzene-hexane. Benzene sulphonic anhydride was prepared in a similar way, absolute ether being used for the recrystallisation. p-Chloro, p-bromo-, and p-iodo benzene sulphonic anhydrides were prepared by direct sulphonation of the halobenzenes (analytical grade from Fluka and British Drug Houses) with sulphur trioxide in nitromethane, and subsequently recrystallised from nitromethane. m-Nitrobenzene sulphonic anhydride was prepared from the corresponding sulphonyl chloride (British Drug Houses). The chloride was hydrolyzed in boiling water; after evaporation (finally in vacuo) the anhydrous acid was transformed into the sulphonic anhydride by thionyl chloride as described above. The product was recrystallised from benzene.

The identity of the anhydrides was checked by titration with alkali and by determination of the melting points in capillary tubes. The results are given below together with calculated values

		\mathbf{H}	$p ext{-} ext{CH}_3$	$p ext{-Cl}$	$p ext{-}\mathrm{Br}$	p-I	$m\text{-NO}_2$
Equiv. wt	. found	151	164	185	228	278	202
Equiv. wt	. calc.	148	163	184	228	275	194
m.p.	\mathbf{found}	$86 - 89^{\circ}$	$115 - 125^{\circ}$	$136 - 142^{\circ}$	$179 - 181^{\circ}$	$215 - 218^{\circ}$	$140 - 155^{\circ}$
m.p.	reported	91.5° a	131.5° a	141° ^b	182° ^b	221° b	160° c

^a Ref. 2 ^b Ref. 7 ^c Ref. 8.

No chloride could be detected by Ag⁺ in the aqueous solutions of the hydrolyzed sulphonic anhydrides.

The sulphonic anhydrides were stored as crystals over phosphorus pentoxide in a vacuum desiccator. Solutions of anhydrides in acetone or dioxan were made up immediately before use.

Description of apparatus. The stopped-flow apparatus was made of glass with connec-

tions of polythene and silicone-rubber tubing.

A diagram of the apparatus is shown in Fig. 1. A is a twin glass-syringe consisting of two 5 ml Chance Interchangeable syringes. The two pistons are rigidly connected. Connection from each syringe can be established through 2 three-way valves, B, either to a reservoir C, or to the mixing chamber D. Connections and valves have 1.5 mm bore. The mixing chamber has a 3.5 mm inner diameter, and the inlets are arranged tangentially. The mixer is connected to a conductivity cell, E, consisting of three platinum rings mounted on the inside of a 4 mm glass tube (Radiometer, Copenhagen, cell type 114, cell constant 0.62 cm). The cell is loaded by an a-c voltage of 0.2 volt and 3 kc/sec, supplied

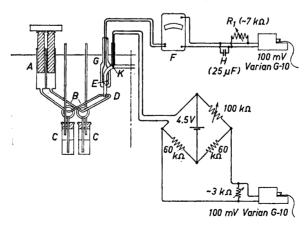


Fig. 1. Diagram of stopped-flow apparatus.

by the oscillator of the conductivity meter, F. The cables from the platinum rings are protected by an outer glass jacket G. The effective volume of mixing has been estimated to 0.05 ml. With the normal rate of injection, 3 ml/sec, the mixing time is therefore 0.017 sec. Full advantage cannot be taken of this short time, because 0.7 ml of mixture must be injected in order to cover the platinum rings. On this account the first 0.23 sec after mixing cannot be investigated.

From the conductivity meter F (Radiometer type CDM 2d) a signal is taken out to a 100 mV recorder (Varian G-10). By means of the resistance R₁, the recorder deflection may be adjusted relative to conductivity. The ripple voltage of the signal is smoothened by the condenser, H, of $25~\mu\text{F}$. The maximum paper speed is 0.6~cm/sec, the paper width is 13~cm, the maximum pen speed when applying a fullspan step function is 18~cm/sec. Although this balancing time is too slow to permit full-scale recording of reactions having firstorder rate constants higher than 1.5 sec-1, it is still possible to trace the last part of runs of reactions having rate constants up to about 4 sec-1, since this corresponds to the pen response when applying a step function corresponding to 1/3 or less of the full span.

The temperature of the reacting mixture was measured with a 100 kohm thermistor, K, placed as close as possible to the outlet of the conductivity cell. The recording of the temperature was done automatically by means of a bridge and a Varian recorder. Changes up to 2° in temperature at the outlet of the cell could be detected within 2 sec with an

accuracy of $\pm 0.05^{\circ}$.

During the experiments the syringes, reservoirs, mixer and conductivity cell were immersed in a water bath thermostated to within $\pm 0.05^{\circ}$. Isothermal conditions are, however, hardly possible to achieve with fast reactions. In the present investigation the main difficulty is the heat of mixing of water and acetone. By mixing equal volumes of acetone and water the temperature will increase several centigrades, but when such 50 vol.% mixture again is mixed with an equal volume of acetone of the same temperature, a negative heat effect is observed. There is a point where no heat is absorbed or evolved, and experiments showed that this is 61.2 vol.% water in acetone mixed with an equal volume of acetone. Similarly, equal volumes of pure dioxan and 70.6 vol.% water in dioxan did not show any heat effect at mixing.

Since it was not possible to measure the temperature in the centre of the conductivity cell, and since it cannot be assumed that the temperature recorded at the outlet of the cell provides a reliable measurement for the reaction temperature when the heat of mixing becomes appreciable, most runs were made using the solvents 30.6 vol.% water in acetone and 35.3 vol. % water in dioxan. (Percentages are given by volume prior to

mixing at 25°).

Procedure for measurements. After rinsing the apparatus with pure acetone and after excluding air bubbles, the one reservoir was filled with the solution of anhydride, and the other with the aqueous solution. The syringes were repeatedly filled from the reservoirs and discharged through the mixer before measurements were started. The concentration of the anhydride solution were usually adjusted to give an equilibrium conductivity of $350-450~\mu \rm mho$, and the recorder was calibrated to give zero deflection for zero conductivity, and 90 % of full-scale for 450 $\mu \rm mho$.

About $3-5~\rm ml$ of reaction mixture were then discharged manually into the conductivity.

tivity cell by applying a firm, sharp push on the pistons. The conductivity recorder instantaneously reacted to show a low reading showing that the liquid in the cell had been displaced by a fresh mixture of reactants. As soon as the push was released the conductivity increased due to the increasing concentration of sulphonic acid in the cell. When the reading had become constant the measurement was repeated by a new discharge from the syringes. At least 3, and usually 6-9 runs were made for a given set of parameters.

Analysis of recorded curves. From the recorded curves, see Fig. 2, 8-15 readings were taken at equidistant time intervals, an early value (less than 0.5 sec after mixing) being selected as zero time. The readings were transformed to concentrations (C) by means of a calibration curve (cf. below), and the values of log $(C_{\infty}-C)/(C_{\infty}-C_0)$ were plotted versus time. From the slope of the plot the pseudo first order rate constant k was calculated. Average values of k, together with standard deviations and numbers of repeated runs, have been presented in Table 1.

Six calibration plots, relating recorder readings to acid concentrations, were made with series of solutions of p-toluene sulphonic acid and p-bromobenzene sulphonic acid

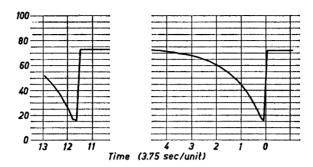


Fig. 2. Automatically recorded curves for hydrolysis of 3.00×10^{-3} M $(p\text{-BrC}_{\bullet}\text{H}_{4}\text{SO}_{2})_{2}\text{O}$ in 30.6 vol.% water in acetone at 16.0°C .

having normalities $10^{-4}-7\times10^{-3}$ in the solvents 30.6 vol.% water in acetone and 35.3 vol.% water in dioxan, at 15°, 25°, and 35°. The deviations from linearity of the calibration curves were appreciable, partly due to a nonlinear recording of the conductivity signal, partly due to the fact that the conductivity is not proportional to the concentration of a strong acid in these solvents (cf. Ref. 9). The variations in rate constants found by applying different calibration plots to one and the same run was about 1% relative, which is not more than the uncertainty in the graphical determination of the rate constant.

Check of apparatus. Measurements were made on the hydrolysis of acetyl chloride (analytical grade from Merck, refluxed and distilled) in 30.6 vol.% water in acetone at 15.3°. A rate constant for the same compound, solvent composition and temperature was extrapolated from data reported by Cairns and Prausnitz. The extrapolated figure is $1.15 \pm 0.07~{\rm sec^{-1}}$, which is in satisfactory agreement with the result obtained in this investigation, $1.12 \pm 0.03~{\rm sec^{-1}}$.

RESULTS AND DISCUSSION

Pseudo first order kinetics. Typical plots are shown in Fig. 3. The linearity of the plots to at least 95 % hydrolysis classifies the kinetics as first order with respect to the substrate. In a number of runs the initial concentration of the substrate was the parameter varied. From the results given in Table 2,

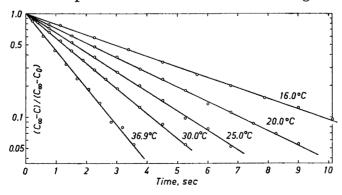


Fig. 3. First order plots for the hydrolysis of bromobenzene sulphonic anhydride in 30.6 vol.% water in acetone at various temperatures.

Table 1. Rate data for hydrolysis of sulphonic anhydrides in 30.6 vol.% water in acetone (I) and in 35.3 vol.% water in dioxan (II)

	. ,		, •	*	, ,	
Init. conc. of substrate $10^3 \times \text{mole/litre}$	Temp.°C	Rate consta	nt	Standard deviation	Number of runs	•
(p-CH ₃ C ₆ H ₄ SO ₂) ₂ C	O(I)					
3.06	16.0	0.0167	土	0.0008	5	
-	20.5	0.0258	主	0.0013	5	
	25.0	0.0331	±	0.0007	6	$\Delta H^{\pm} = 12.3 \text{ kcal}$
<u></u>	29.8	0.051	主	0.003	3	$\Delta S^{\pm} = -24.2 \text{ e.u.}$
	35.0	0.071	土	0.003	6	25 24.2 c.u.
0.31	42.1	0.105	土	0.008	. 4	
(C H 80) O(I)						
$(C_6H_5SO_2)_2O(I) = 3.02$	15.0	0.0388	,	0.0013	6	
3.02			土			
	20.0	0.0547	<u>+</u>	0.0011	9	477+ 11.011
	25.0	0.0763	±	0.0012	6	$\Delta H^{\ddagger} = 11.0 \text{ kcal}$
	29.9	0.1062	±	0.0023	5	$\Delta S^{\pm} = -26.7 \text{ e.u.}$
	34.8	0.139	<u>±</u>	0.006	6	
$(p\text{-ClC}_{6}\mathbf{H}_{4}\mathbf{SO}_{2})_{2}\mathbf{O}($	I)					
3.25	15.0	0.200	\pm	0.007	7	
_	20.0	0.282	\pm	0.004	7	$\Delta H^{\ddagger} = 10.4 \text{ kcal}$
	25.0	0.395	\pm	0.006	7	$\Delta S^{\pm} = -25.7 \text{ e.u.}$
	30.1	0.503	土	0.013	5	
	34.8	0.677	主	0.026	6	
${(p\text{-BrC}_{6}\text{H}_{4}\text{SO}_{2})_{2}\text{O}_{6}}$	/T)	***************************************				
		0.090		0.005	6	
3.00	16.0	0.239	±	0.005		477
	20.5	0.326	±	0.007	6	$\Delta H^{\pm} = 10.5 \text{ kcal}$
	25.0	0.429	土	0.005	3	$\Delta S^{\pm} = -24.9 \text{ e.u.}$
	30.0	0.579	土	0.017	5	
	36.8	0.88	<u>±</u>	0.03	6	
$(p\text{-}\mathrm{IC_6H_4SO_2})_2\mathrm{O(I}$)					
3.00	15.0	0.212	\pm	0.006	6	
_	20.0	0.282	主	0.009	6	$\Delta H^{\ddagger} = 10.3 \mathrm{kcal}$
	25.0	0.373	主	0.024	$\ddot{6}$	$\Delta S^{\pm} = -25.8 \text{ e.u.}$
_	30.0	0.528	土	0.015	6	20.0 c.u.
	35.0	0.706	± +	0.013	6	
		0.706		0.023	0	
$(m ext{-} ext{NO}_2 ext{C}_6 ext{H}_4 ext{SO}_2)_2$	$_{2}O(I)$	2 7 2		0.10		
10.0	15.2	2.56		0.13	3	
CH ₃ COCl (I)						
7.0	15.3	1.12	土	0.03	7	
(p-CH ₃ C ₆ H ₄ SO ₂) ₂ (O(II)					
3.07	16.0	0.0229	土	0.0014	3	$\Delta H^{\ddagger} = 13.2 \text{ kcal}$
0.0.	25.0	0.0455	主	0.0026	4	$\Delta S^{\pm} = -20.4 \text{ e.u.}$
, 	33.8	0.0433 0.0921		0.0013	4	26. = -20.4 e.u.
		0.0921		0.0013	**	
$(p\text{-BrC}_6\mathrm{H}_4\mathrm{SO}_2)_2\mathrm{O}_2$	$^{(II)}$	0.555		0.00=	_	
3.00	16.0	0.232	土	0.005	3	
_	20.5	0.331	土	0.007	7	
	25.0	0.442	±	0.013	6	$\Delta H^{\ddagger} = 11.3 \text{ kcal}$
;	29.9	0.627	\pm	0.017	7	$\Delta S^{\pm} = -22.0 \text{ e.u.}$
		0.844		0.021	7	
· _	34.X	U.044				
* <u>=</u>	$\frac{34.8}{39.8}$	1.097	土土	0.021	6	

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7

0.89

0.66

0.89

No.	Init.conc. 103 M	Added electrolyte	Rate constant sec ⁻¹
	10 101	Auded electrory to	Trate constant sec
1	3.01	0	0.432 ± 0.015 (7)
2	1.50	0	0.426 + 0.005 (8)
3	0.66	0	0.438 + 0.027 (9)
4	0.66	0.010 M NaCl	$0.449 \pm 0.030 (7)$
5	0.66	0.010 M LiCl	0.457 ± 0.015 (8)
			

0.010 M Na-bromobenzenesulphonate

0.005 M bromobenzenesulphonic acid

0.010 M NaOH

Table 2. Rate data for hydrolysis of p-bromobenzenesulphonic anhydride in 30.6 vol.% water in acetone at 25.0°.

experiments Nos. 1—3, it will be seen that no significant change in the rate constant is observed. This corroborates the first order kinetics.

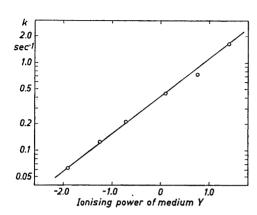
Effect of added electrolytes. In a number of runs the effect of adding electrolytes to the reaction mixture was studied, cf. Table 2. The absence of acid catalysis shows that the hydrolysis in acid and neutral solutions is produced by neutral water molecules. The concentration of water in the solvent investigated is 17 mole per liter. By expressing the second order hydrolysis constant as $k_2 = k_1/[\mathrm{H_2O}]$, k_2 for hydrolysis by water molecules is calculated to be $2.5 \times 10^{-2} \, \mathrm{l \cdot sec^{-1}}$ mole⁻¹. The corresponding value for hydrolysis produced by hydroxyl ions is $\geq (1.4-0.4)/0.01 = 10^2 \, \mathrm{l \cdot sec^{-1}}$ mole⁻¹. This marked increase in rate of hydrolysis caused by hydroxyl ions is in accordance with an $\mathrm{S_{N}2}$ substitution but does not correspond to an $\mathrm{S_{N}1}$ ionization. The small, barely significant increase in rate caused by the addition of a common-ion salt as well as of a non-common-ion salt also points towards an $\mathrm{S_{N}2}$ mechanism, cf. Ref. 10, p. 362. This $\mathrm{S_{N}2}$ mechanism is in perfect agreement with previous results from studies on the hydrolysis of sulphonyl chlorides in similar mixed solvents.¹

Influence of solvent composition. The results showing the influence of varying the water concentration on the hydrolysis rate of p-bromobenzene sulphonic anhydride at 25° can be presented in a diagram with $\log k$ as ordinate and log molar water concentration as abscissa. The plot (not shown) is fairly linear with a slope of 1.75. Since the water constitutes a high proportion of the solvent, this result cannot be rationalised simply in terms of molecularity of the reacting water. It is, however, of interest that slopes of 1-2 usually signify S_N^2 reactions, whereas S_N^1 reactions normally show slopes of 5-7.1 An alternative way of representing these data have been shown in Fig. 4. In this diagram the log k values have been plotted versus the ionising power of the medium, Y, as defined by Grunwald and Winstein; cf. Ref. 11, p. 297. The plot shows a good linear correlation with a slope m=0.42. The fact that the m value does not increase when increasing the water content suggests that the S_N2 mechanism operates over the whole range from 10 to 50 vol. % water in acetone. It is of interest to note that the m value to be derived from the data of Vizgert for the S_N2 hydrolysis of sulphonyl chlorides in dioxanwater mixtures at least up to 40 % water also is 0.42 (cf. Ref. 1, Fig. 5).

 0.450 ± 0.040 (7)

>1.40

 $0.445 \pm 0.017 (10)$



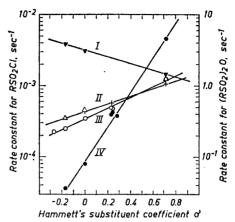


Fig. 4. Rate data for the hydrolysis of bromobenzene sulphonic anhydride at 25.0° in dependence of the solvating power of the medium as defined by Grunwald-Winstein 11 for various mixtures of water and acetone.

Fig. 5. Plots of log k against Hammett's substituent coefficients σ_i^{12} for the hydrolysis of sulphonyl chlorides and sulphonic anhydrides. I: RSO₂Cl in pure water at 25° (Hedlund ¹³). II: RSO₂Cl in 50 % water in acetone at 30° (Linetskaya ¹⁴ + and Hedlund ¹³ \triangle). III: RSO₂Cl in 30 % water in dioxan at 50° (Vizgert ¹). IV: (RSO₂)₂O in 30.6 vol.% water in acetone at 25° (this work). The value for $(m\text{-NO}_2\text{C}_6\text{H}_4\text{SO}_2)_2\text{O}$ has been extrapolated from the rate at 15° assuming $\Delta H^{\pm} = 10$ kcal.

Influence of ring substituent. According to Hammett ¹² the rate constant k for a reaction involving a substituted compound may often be related to the rate constant k_0 for the same reaction of the corresponding unsubstituted compound by the equation: $\log k - \log k_0 = \varrho \times \sigma$. Here, ϱ is a reaction constant independent of the nature of the substituent but characteristic of the type of reaction, while σ is a substituent constant independent of reaction type. The latter constant is defined as the logarithm of the ratio of the ionization constant of the similarly substituted benzoic acid to the ionization constant of unsubstituted benzoic acid.

In Fig. 5 the logarithm of rate constants for the hydrolysis of sulphonyl chlorides and sulphonic anhydrides have been plotted against Hammett's substituent coefficients, σ . Each of the four series shows a linear relationship with different slopes, corresponding to different ϱ -values.

For the hydrolysis of sulphonyl chlorides in pure water an S_N1 mechanism has been inferred:¹

$$RC_6H_4SO_2Cl \Longrightarrow RC_6H_4SO_2^+ + Cl^-$$
 (rate determining) (1)

$$RC_{6}H_{4}SO_{2}^{+} + H_{2}O \longrightarrow RC_{6}H_{4}SO_{3}H + H^{+}$$
 (fast) (2)

The negative slope (ϱ) of the data for pure water should be expected, for the quantity — σ measures the increase in electron density at the reaction site produced by the substituent R, and the rate determining ionization according to the above equation must be favoured with increasing electron density at the sulphur atom.

When the hydrolysis of the sulphonyl chlorides proceeds by an S_N^2 substitution, as is inferred 1 for the mixtures of water and acetone or dioxan:

$$RC_{6}H_{4}SO_{2}Cl + H_{2}O \Longrightarrow RC_{6}H_{4} - \overset{O}{\overset{\bullet}{S}} \longrightarrow RC_{6}H_{4}SO_{3}H + H^{+} + Cl^{-}$$
(3)
$$Cl \longrightarrow RC_{6}H_{4}SO_{3}H + H^{+} + Cl^{-}$$
(4)
$$Cl \longrightarrow RC_{6}H_{4}SO_{3}H + H^{+} + Cl^{-}$$
(5)

the effect of decreasing σ will still be to ease rupture of the S—Cl bond, but another effect will tend to balance the former, namely the increasing resistance against nucleophilic attack from the water molecule. It follows therefore that the ϱ value for such hydrolysis should become less negative or even positive, and the data presented in Fig. 5 confirm this conclusion.

Turning now to the hydrolysis of sulphonic anhydrides, and assuming an $S_n 2$ mechanism for this process

$$(RC_{6}H_{4}SO_{2})_{2}O + H_{2}O \Longrightarrow RC_{6}H_{4} - \underbrace{\overset{O}{\underset{5}{\downarrow}}}_{S}\overset{O_{3}SC_{6}H_{4}R}{(A)} \longrightarrow 2 RC_{6}H_{4}SO_{3}H \quad (4)$$

$$(transition state)$$

it may be noticed when comparing (4) with (3) that there are now two additional effects from the substituent in the leaving anion (A) to be taken into account. Firstly, decreasing σ -values will give an extra contribution to the electron density at the reaction site to repel water attack. Secondly, increasing σ -values will favour the formation of the anion A. Both effects should raise the ϱ -value, in accordance with the experimental data.

Absolute values of rate constants. From the data relating to mixed solvents in Fig. 5 it will appear that the rate of hydrolysis is 100—4000 times faster for the anhydrides than for the chlorides. Although the media used for the investigations are not strictly identical it may safely be concluded that such large differences must be ascribed to the different substrates. The qualitative experience concerning the higher reactivity of the sulphonic anhydrides compared to the sulphonyl chlorides² has therefore been confirmed.

It is of interest to know whether this difference is enthalpy or entropy controlled. For each set of runs Arrhenius plots were made, some of which are shown in Fig. 6. From the slope of these plots the energies of activation E cal were calculated, and from E and the rate constant at 25° the value of $\log A$ of the Arrhenius equation was obtained ($\log A = \log k + E/T \times 4.575$). Finally ΔH^{\pm} , the enthalpy of activation, and ΔS^{\pm} , the entropy of activation,

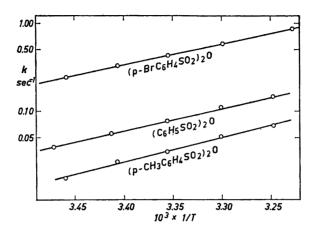


Fig. 6. Arrhenius plots for the hydrolysis of various sulphonic anhydrides in 30.6 vol.% water in acetone.

were calculated for each component, ΔH^{\pm} (cal) = E - 600 and ΔS^{\pm} (e.u.) = $4.575 \times \log A - 60.53$, cf. Ref. 11, p. 71. Both activation parameters are included in Table 1.

In Table 3 some values of ΔH^{\pm} (in kcal) and ΔS^{\pm} (in e.u.) have been compiled. Unfortunately none of the available data for the two types of compounds relates to identical solvent composition. Under this circumstance it appears that the best comparison possible should be between the data in column III and in column IV. It may be argued that the difference in ΔG^{\pm} caused by the difference between 30 % water in dioxan and 30 % water in acetone is small. Thus the solvolysis rate constant at 25° for t-butyl chloride is 1.31 times greater in the latter than in the former solvent, 11 corresponding

Table 3. Activation parameters for hydrolysis of sulphonyl chlorides and sulphonic anhydrides.

I: RSO₂Cl in pure water (Hedlund ¹³)

II: RSO₂Cl in 50 % water in acetone (Linetskaya ¹⁴ and Hedlund ¹³)
III: RSO₂Cl in 30 % water in dioxan (Vizgert ¹)
IV: (RSO₂)₂O in 30.6 vol.% water in acetone (this work)
V: (RSO₂)₂O in 35.3 vol.% water in dioxan (this work).

R	ΔH^{\pm} keal					<i>∆S</i> ‡ e.u.				
	I	II	III	IV	v	I	II	III	IV	v
$p ext{-} ext{CH}_3 ext{C}_6 ext{H}_4$	17.4	13.7	13.2	12.2	13.2	-11.3				
C ₆ H ₅	16.8	13.8 13.3	12.8 11.7	11.0 10.4	_	-13.5	-28.5 -29.5		$-26.7 \\ -25.7$	
$p\text{-CH}_3\text{C}_6\text{H}_4$ C_6H_5 $p\text{-ClC}_6\text{H}_4$ $p\text{-BrC}_6\text{H}_4$	_	13.3	11.7	10.4	11.3	_	-29.5		-25.7 -24.9	1

to a difference in ΔG^{\pm} of 0.16 kcal. Furthermore, the rate constant for the hydrolysis of p-toluenesulphonyl chloride at 30° is only 1.15 times greater in from the free three suppositions of p-tordenestiphonyl chloride at 50 is only 1.15 times greater in 50 % water in acetone than in 50 % water in dioxan (calculation based on data reported by Hedlund ¹³ and Vizgert ¹). In spite of these examples, it is not certain that differences in ΔS^{\pm} and ΔH^{\pm} will be small. Therefore some runs were made with anhydrides in 35.3 vol. % water in dioxan (it was impossible to avoid a heat effect when using 30 vol. % water in dioxan). The results are shown in columns V in the table, and it will appear that they do not deviate greatly from the results in columns IV. A direct comparison between columns III and columns IV is therefore permissible. It will be seen that the greater rate in the anhydride hydrolysis is mainly caused by a higher ΔS^{+} , the difference being of the order of 10 e.u. This difference is due most probably to differences in the change of structure of the solvent shell during the transformation of the less polar reactants to the more polar transition states. The solvation entropy of the benzenesulphonate ion has not been measured, but it may be indicative that the partial molal entropies for the aqueous hydrogensulphate ion, HSO_4^- , and for the aqueous hydrogensulphite ion, HSO₃, are 32.6 and 30.6 e.u., respectively. 15 The corresponding value for the chloride ion is only 13.5 e.u; thus it appears that the difference in reaction rates can be rationalised in terms of solvation effects of the transition states.

The somewhat different values for the chloride data in pure water, col. I, bear out the different mechanism operating in this solvent. It is not unlikely that a shift in mechanism also will be observed in the anhydride hydrolysis, when the water content is increased above 50 vol.%.

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